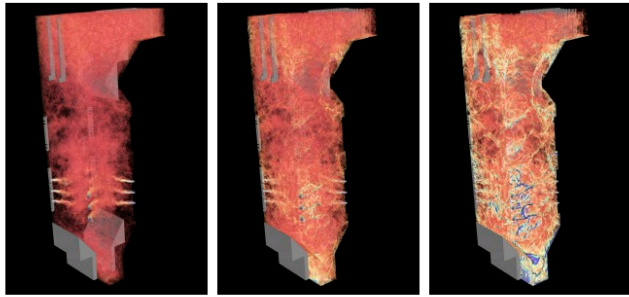


Coal Particle Combustion

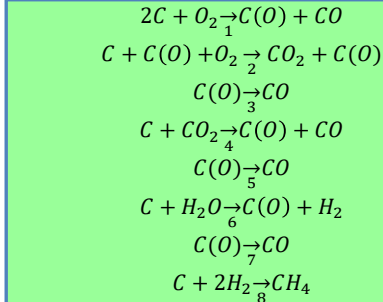
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Brigham Young University, Provo, UT
SSAP Symposium 2015, Santa Fe, NM



Small (30 μm) particles. Medium (60 μm) particles. Large (90 μm) particles.

Char Conversion

- Complex surface chemistry
- Heat of rxn
- External and pore diffusion
- Sintering, ash inhibition

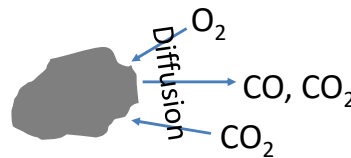


• CBK Features (from Hurt)

- Decreasing rate with increasing conversion
- Annealing, ash inhibition
- Originally included statistical kinetics
- Effectiveness factor for pore diffusion
- Particle size distribution

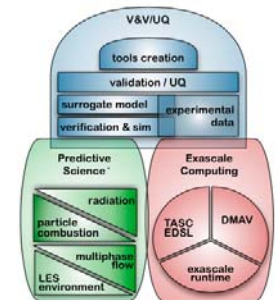
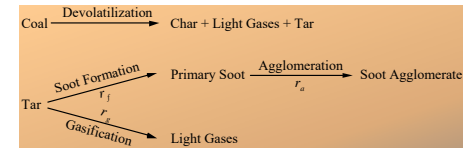
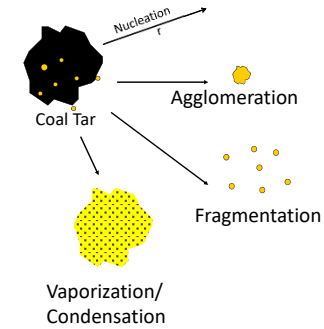
• Char Conversion Kinetics (CCK)

- Based on CBK/E and CBK/G (from Liu and Niksa)
- Multiple surface reactions
- Multi-component transport
- Random pore model
- Global sensitivity analysis
- Generate a surrogate model



Soot

- Coal tar soot is different than soot from light gases
- Soot in flame regions can radiate significant amount of heat away from flame to walls
- Soot mainly comes from coal tar, but at high temperatures acetylene becomes more important
- Alex Brown's soot model implemented in Arches



Carbon Capture Multidisciplinary Simulation Center (CCMSC) team structure.

Pyrolysis

- CPD model predicts volatiles and tar as function of coal type, T, and dT/dt
- Surrogate pyrolysis model needed

Solution: Modified 2-step

$$\frac{d(\alpha_{coal})}{dt} = -(F_1 k_1 + F_2 k_2) \alpha_{coal}$$

$$\frac{d(\alpha_{vol})}{dt} = (F_1 Y_1 k_1 + F_2 Y_2 k_2) \alpha_{coal}$$

$$F_n = e^{(\sum_{i=0}^5 c_{i,n} [X_v]^i)}$$

$$\frac{d(\alpha_{tar})}{dt} = (F_{1,tar} Y_{1,tar} k_{1,tar} + F_{2,tar} Y_{2,tar} k_{2,tar}) \alpha_{coal}$$

- Can fit CPD model predictions of volatiles well for multiple heating rates heating rate

